

## 1. 40 points.

(a) Draw a line connecting the statement on the left with the most appropriate explanation on the right.

- $\Delta_{\text{mix}}S > 0$  because D  $S$  increases with  $V$  for each substance
- $\Delta_{\text{vap}}H$  decreases with  $T$  because A  $C_{Pm}$  is bigger for the liquid than for the gas
- vapor pressure increases with  $T$  because C more energy per molecule is available to break intermolecular bonds
- water has a higher  $T_f$  than propane because B dispersion forces are generally weaker than hydrogen bonds
- water melts at a constant  $T$  as heat is added because E the average energy per degree of freedom remains constant

(b) The boiling point for isobutane (2-methylpropane) is 261.3 K. Use Trouton's rule to estimate the standard enthalpy of vaporization. **Solution:** Trouton's rule predicts that  $\Delta_{\text{vap}}S_m^\ominus$  is roughly  $8R$  to  $13R$ , so  $\Delta_{\text{vap}}H_m^\ominus = T_b^\ominus \Delta_{\text{vap}}S_m^\ominus$  should be between 17 and 28 kJ mol<sup>-1</sup>. The actual value is 21.3 kJ mol<sup>-1</sup>.

(c) From the phase diagram for isobutane, give  $T$  and  $P$  for

i. the critical point: 408 K, 36 bar

ii. the triple point: 114 K, 0.02 bar

iii. the standard state melting point: 114 K, 1.0 bar

2. Find an expression for each of the following in terms of  $\Delta_{\text{vap}}H_m^\ominus$  and  $T_b^\ominus$  or their derivatives:

(a)  $\Delta_{\text{vap}}E_m^\ominus$

$$= \Delta_{\text{vap}}H_m^\ominus - \Delta_{\text{vap}}(P^\ominus V_m) \approx \Delta_{\text{vap}}H_m^\ominus - P^\ominus V_m(g) = \boxed{\Delta_{\text{vap}}H_m^\ominus - RT_b^\ominus}$$

(b)  $\Delta_{\text{vap}}F_m^\ominus$

$$= \Delta_{\text{vap}}E_m^\ominus - T_b^\ominus \Delta_{\text{vap}}S_m^\ominus = (\Delta_{\text{vap}}H_m^\ominus - RT_b^\ominus) - \Delta_{\text{vap}}H_m^\ominus = \boxed{-RT_b^\ominus}$$

(c)  $\Delta_{\text{vap}}\mu^\ominus$  at constant  $S$

$$= \Delta_{\text{vap}} \left( \frac{\partial H}{\partial n} \right)_{S, P^\ominus} = \boxed{\Delta_{\text{vap}}H_m^\ominus} \text{ at constant } S.$$

(d)  $C_{Pm}(g) - C_{Pm}(l)$  at  $T_b^\ominus$  and 1 bar

$$\begin{aligned} &= \left( \frac{\partial H_m(g)}{\partial T} \right)_{P^\ominus, n} - \left( \frac{\partial H_m(l)}{\partial T} \right)_{P^\ominus, n} \Big|_{T_b^\ominus} = \left( \frac{\partial H_m(g) - H_m(l)}{\partial T} \right)_{P^\ominus, n} \Big|_{T_b^\ominus} \\ &= \left( \frac{\partial \Delta_{\text{vap}}H_m^\ominus}{\partial T} \right)_{P^\ominus, n} \Big|_{T_b^\ominus} \end{aligned}$$

3. It takes a  $17.3 \text{ J K}^{-1}$  change in entropy to heat  $0.300 \text{ mol}$  of glycerol from a solid at  $T_f^\ominus = 291 \text{ K}$  to a liquid at  $331 \text{ K}$ . The heat capacities are  $150 \text{ J K}^{-1} \text{ mol}^{-1}$  for the solid and  $221.9 \text{ J K}^{-1} \text{ mol}^{-1}$  for the liquid. Find  $\Delta_{\text{fus}}H_m^\ominus$ . **Solution:** This is a two-step process, and we can write expressions for the entropy change at each step. The  $\Delta_{\text{fus}}H_m^\ominus$  is then related to the  $\Delta_{\text{fus}}S_m^\ominus$  by the temperature  $T_f^\ominus$ :

$$\begin{aligned}\Delta S &= \Delta S_{\text{vaporization}} + \Delta S_{\text{heating liq}} \\ &= n \frac{\Delta_{\text{fus}}H_m^\ominus}{T_f^\ominus} + nC_{Pm}(l) \ln \frac{T_f^\ominus}{T_1} \\ \Delta_{\text{fus}}H_m^\ominus &= T_f^\ominus \left[ \frac{\Delta S}{n} - C_{Pm}(l) \ln \frac{T_f^\ominus}{T_1} \right] \\ &= (291 \text{ K}) \left[ \frac{17.3}{0.300} - (221.9) \ln \frac{331}{291} \right] (\text{J K}^{-1} \text{ mol}^{-1}) \\ &= \boxed{8.46 \text{ kJ mol}^{-1}}.\end{aligned}$$

4.  $\text{OsO}_4$  sublimes ( $\Delta_{\text{sub}}H_m^\ominus = 56.9 \text{ kJ mol}^{-1}$ ) with vapor pressure of  $0.013 \text{ bar}$  at  $298 \text{ K}$ . Estimate the vapor pressure at  $325 \text{ K}$ . **Solution:** The Clausius-Clapeyron equation is partly based on the idea that the volume change upon vaporization is essentially equal to the volume of the gas that forms. This assumption applies just as well to sublimation, where we go from the solid to the gas directly. Although we don't have the boiling point, we can integrate the differential form of the Clausius-Clapeyron equation (Eq. 20.36) from any lower limit, in this case  $P=0.013 \text{ bar}$  and  $T = 298 \text{ K}$ :

$$\begin{aligned}\int_{0.013 \text{ bar}}^P d \ln P' &= -\frac{\Delta_{\text{sub}}H_m^\ominus}{R} \int_{298 \text{ K}}^{325 \text{ K}} d \left( \frac{1}{T'} \right) \\ \ln \frac{P}{0.013 \text{ bar}} &= \frac{\Delta_{\text{sub}}H_m^\ominus}{R} \left( \frac{1}{298 \text{ K}} - \frac{1}{325 \text{ K}} \right) = 1.908 \\ P &= (0.013 \text{ bar})e^{1.908} = \boxed{0.088 \text{ bar}}.\end{aligned}$$